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## **CHEMICAL ENGINEERING REFRESHER PROGRAM**

## HEAT TRANSFER AND EVAPORATION

			USI IR AID IVAL OR		
1.		ensionless ratio is used to determin ered a thermally developed fluid.	e the thermal development on the e	entra	nce to ducts where a value of less than 1000
	a.	Grashof number		C.	Graetz number
	b.	Eckert number		d.	Stanton number
2.	What is i	nstalled to prevent tube damage fro	om incoming high-velocity shell inlet	t flui	d?
	a.	impingement baffle		C.	spacer
	b.	bar baffle		d.	tie rod
3.	What is t		be sheet exchanger with removable	e ch	annel and cover, bonnet type rear head, and
	a.	DGS		C.	BEN
	b.	CKT		d.	AFM
4.	thin-walle	ed 2-cm-diameter tubes at 80 °C a	nd leaves at 40 °C. Determine the L	MT	
	a.	32.66 K		C.	24.66 K
	b.	27.44 K		d.	22.44 K
4,340 kV water are	Vusing bra 27.8 and	ackish water. Cooling water inlet to 68.9 kg/s, respectively. Titanium p	emperature is at 25 °C and outlet te	mpe on. T	of methanol from 95 °C to 40 °C with duty of erature at 40 °C. Flow rates of methanol and The logarithmic mean temperature difference W/m-K.
5.	What is t	he required total heat transfer area	ı in m²?		
	a.	62.29		C.	82.35
	b.	92.04	(	d.	72.92
6.		an effective plate area of 0.75 m <sup>2</sup> is the channel velocity of methano		plate	e spacing at 3 mm, and number of passes of
	a.	0.61		C.	0.41
	b.	0.51	(		0.32
7.	What is t	he channel velocity of brackish wa	ter in m/s?		
	a.	0.85	(	C.	1.32
	b.	0.96	(	d.	2.17

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heating i	s disconti	rubber 1-in thick at an initial nued when the temperature termal diffusivity of 0.0029 ft <sup>2</sup>	at the midplane of the slal	reaches 270 °F	. The thermal co	nductivity of rubber is 0.092
8.	How ma	ny hours is the heating perior	d time?			
0.	a.	1.20	a umo:	C.	0.81	
	b.	0.99		d.		
9.		the temperature in °F of the i	rubber if it is 0.25 in from th			
	a.	274.0		C.	270.4	
	b.	247.0		d.	240.7	
10.	How Ion	g will it take in hours for the r	rubber to reach a temperatu	re of 270 °F?		
	a.	~ ~ - ~ ~		C.	0.744	
	b.	0.694		d.	0.964	
	meter tub	asses and 8-tube passes he es. The shell has an inside o				
11	Determin	ne the total tube side crossflo	ow area in cm²			
11.	a.	28.9	JW alea III CIII	C.	98.2	
	b.	74.5		d.	57.4	
	٠.	1 119		4	0	
12.	Determin	ne the total shell side crossflo	ow area in cm <sup>2</sup> .			
	a.	85.0		C.	90.0	
	b.	80.0		d.	95.0	
13.	Which or a. b. c. d.	f the following statements de The boiling point of a soluti There is a linear relationshi The enthalpy of mixing of a There is a non-linear relatio	on is inversely proportional ip between the boiling point concentrated solution is di	of the pure solve rectly proportiona	nt and the solutio I to its concentrat	n for a given pressure.
14	Why is t	hermocompression utilized in	a single-effect evanorator			
17.	a.	To reduce energy requirem				
	b.	To decrease steam econor				
	C.	To reduce fouling in the she		er		
	d.	To increase boiling point ris				
15	What me	odels a perfect diffuse surfac	a that coattors incident illum	ination oqually in	all directions?	
15.	a.	Planck surface	e triat scatters incluent illum	C.	black body	
	b.	gray body		d.	Lambert surfac	Α
	υ.	gray body		u.	Lambort danad	•
16.	This is th	ne type of operation used in t	the evaporation of brine to r	nake salt.		
	a.	forward feed		C.	mixed feed	
	b.	backward feed		d.	parallel feed	
17.	liquid lev	t-type short-tube vertical eva vel is maintained at the top to is concentrated at ambient of 565 495	be sheet. Estimate the ove	rall heat transfer	coefficient in BTU	
	υ.			u.		

18-20. 4 kg/s of a liquor containing 10% wt solids is fed at 294 K to the first effect of a triple-effect unit. Liquor with 50% wt solids is to be withdrawn from the third effect, which is at a pressure of 13 kN/m². The liquor may be assumed to have a specific heat of 4.18 kJ/kg K and to have no boiling point rise. Saturated dry steam at 205 kN/m² is fed to the heating element of the first effect and the condensate is removed at the steam temperature in each effect. The three units are to have equal areas with heat transfer coefficients of 3.1, 2.0 and 1.1 kW/m²-K for the first, second, and third effects, respectively.

1.1 kW/m	n <sup>2</sup> -K for th	e first, second, and third effects, respectively.		
18.	What is tale.	the heat transfer surface area in m <sup>2</sup> of the first effect? 68.75 85.50	c. d.	74.25 64.25
19.	What is tale.	the temperature difference in the second effect? 17.32 K 55.81 K	c. d.	34.57 K 19.60 K
20.	What is tall a. b.	the steam economy of the multi-effect system? 2.00 3.00	c. d.	2.50 1.25
21.		iling mechanism is characterized with a slow initial heat flux rise for in rise significantly due to radiation? nucleate boiling film boiling	ncreas c. d.	natural convection transition boiling
22.	What typ a. b.	e of fouling pertains to the accumulation of organisms that are attra Biofouling freezing fouling	cted to c. d.	o the warm surface? corrosion fouling particulate fouling
23.	Which of a. b.	the following is the best insulator at 300 °C? calcium silicate polyurethane	c. d.	cellular glass mineral wool
24.	Which st a. b. c. d.	atement is false regarding forced-draft air-cooled heat exchanger? It requires less power when air-temperature rise is less than 30 K. The fans are located below the tube bundles and pushes air acros It offers better accessibility to fan maintenance and adjustment. Structural costs are less and mechanical life is longer.		tube surface.
25.	What he a. b.	at exchanger has a series of stacked helical-coil tubes and can be u spiral-plate graphite	used a c. d.	s cryogenic vaporizer? plate-fin tubular spiral-tube
		I gray planes which are very large have emissivities of 0.8 and 0.7 ves, respectively.	vith ter	mperatures of 1100 °F and 600 °F for the first
26.	What is to a.	the net radiation from the first to the second surface in BTU/hr-F°? 3380 5210	c. d.	7960 4750

C.

d.

3380

4750

27. If the surfaces are both black, what is the net radiation in in BTU/hr-F°?

a. 5210

b. 7960

28-30. Air flowing at a 0.90 kg/s is warmed from 283 K to 366 K by passing through pipes of a bank consisting of 20 pipes in each row. The arrangement is in-line with center-center spacing, in both directions, equal to twice the pipe diameter. The heating medium is flue gas with a mass velocity of 10 kg/m²-s; and enters at 700 K and leaves at 366 K, passes across outside of the pipes. For simplicity, the diameter of the outer and inner pipes can be taken as 12 mm. The specific heat capacity of air and flue gas is 1.0 kJ/kg-K. Values for k and  $\mu$  are shown:

	k (W/m-k)µ (mPa-	-s)		
	0.022	0.0165		
	0.044	0.0276		
	0.055	0.0367		
What is	the mass velocity of	f the air inside the pipe in kg/m²-s?		
a.	23.1	•	C.	19.9
b.	29.1		d.	21.9
Calculate	e the overall heat tr	ansfer coefficient in W/m²-K.		
a.	66.5		C.	65.6
b.	67.3		d.	63.7
Neglecti	ng gas radiation, ho	ow long should the pipes be?		
a.	962 m		C.	692 m
	a. b. Calculat a. b.	0.022 0.044 0.055  What is the mass velocity of a. 23.1 b. 29.1  Calculate the overall heat tra. 66.5 b. 67.3  Neglecting gas radiation, ho	0.044 0.0276 0.055 0.0367  What is the mass velocity of the air inside the pipe in kg/m²-s? a. 23.1 b. 29.1  Calculate the overall heat transfer coefficient in W/m²-K. a. 66.5 b. 67.3  Neglecting gas radiation, how long should the pipes be?	0.022

31-32. A 2-tube passes TEMA Class B heat exchanger has: tube bundle outer diameter of 3 ft, baffle spacing and entrance/exit baffle spacing both equal to 8 in, effective length of 14 ft, tube outer diameter of 1 in, and square tube pitch of 1.25 in.

31. Determine the number of baffles.

a. 14

c. 20

d. 629 m

b. 40

b. 926 m

d. 12

32. Estimate the number of tubes.

a. 579

c. 1166

b. 1266

d. 550

33. If the LMTD of a countercurrent heat exchanger cannot easily be determined, which of the following can be used to calculate its heat transfer rate?

a. Planck's law

c. pinch analysis

b. effectiveness-NTU method

d. Biot number

34. Which evaporator is commonly used for concentrating heat-sensitive fruit juices?

a. falling-film

c. short-tube vertical

b. forced circulation

d. horizontal tube

35. Which evaporator has the highest average overall heat transfer coefficient and lowest cost per capacity?

a. horizontal-tube

c. short-tube vertical

b. long-tube vertical

d. agitated thin-film

36-37. A single effect evaporator is to concentrate 20,000 lb/hr of a 20% wt NaOH solution to 50 wt%. The gauge pressure of the steam is 20 psi while the absolute pressure in the vapor space is 100 mm Hg. The overall coefficient is estimated to b 250 BTU/ft²-hr-F° while the feed temperature is 100 °F.

36. Calculate its economy.

a. 0.78

c. 0.99

b. 0.87

d. 0.66

37. Calculate its heating surface required in ft<sup>2</sup>.

a. 1215

c. 864

b. 670

d. 930

38-40. A double-effect evaporator system is to be used to concentrate glycerol-water solution from 10 to 40 percent glycerol by weight at a rate of 1000 kg/h of feed. Identical long-tube natural circulation evaporators are to be used, with overall heat transfer coefficients of 2270 and 1703 W/m²-C° expected for the first and second effects, respectively, when using backward feed. The feed enters at 15 °C while saturated steam at 120°C is used to heat the first effect. An absolute pressure of 115 mm Hg is to be maintained in the second effect. Assume that the specific heat of all solutions is equal to 4.187 J/g-C° and units are to have equal areas.

38. What is the heat transfer surface area in m<sup>2</sup> of the second effect?

a.	4.34	C.	6.22
b.	5.35	d.	3.01

39. What is the steam consumption in kg/h?

a.	525		Ū	C.	478
b.	874			d.	255

40. What is the steam economy of the multi-effect system?

